

ADEM

Savings With Pump Efficiencies

Energy Management Initiative



Tennessee Wastewater Utility Partnership
Wave Five
November 14, 2017

Jim Grassiano – Alabama Department of Environmental Management

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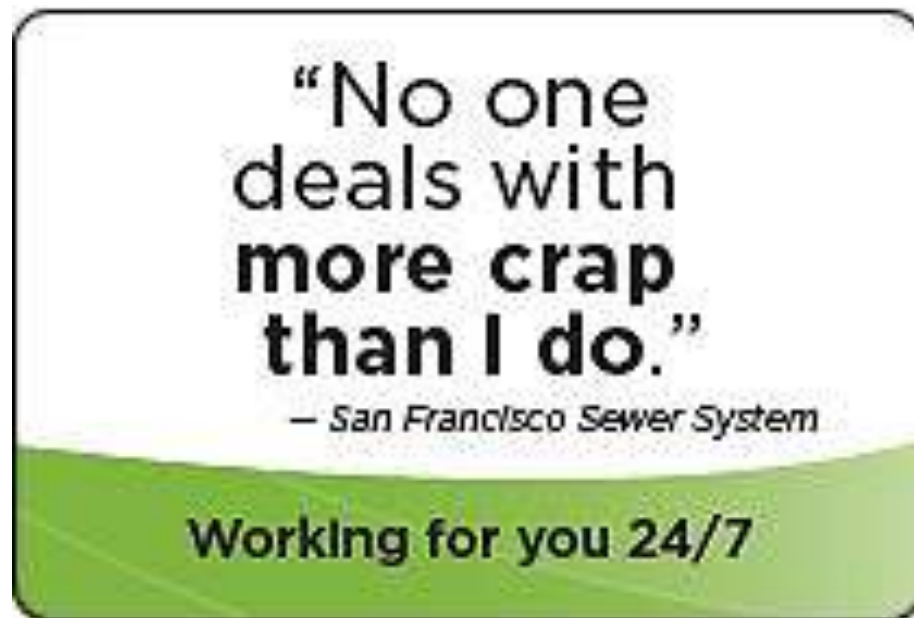
Our Main Job...?



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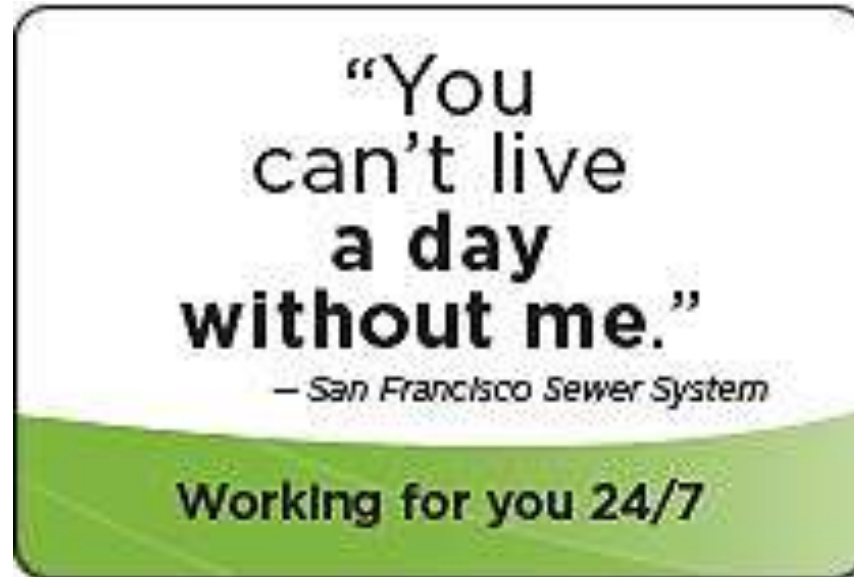


San Francisco Public Utilities PR Campaign





San Francisco Public Utilities PR Campaign





The SFPUC Ads Appeared...

- On bus stops
- In and on city buses
- 14 neighborhood papers
- In Chinese & Spanish
- Larger City-wide papers:
 - *San Francisco Examiner*
 - *San Francisco Bay Guardian*
- Facebook



PR Campaign Intended to foster support for...

- \$2.7 billion dollar, 2-yr upgrade of City WWTPs

(So you think you have budget problems..!)

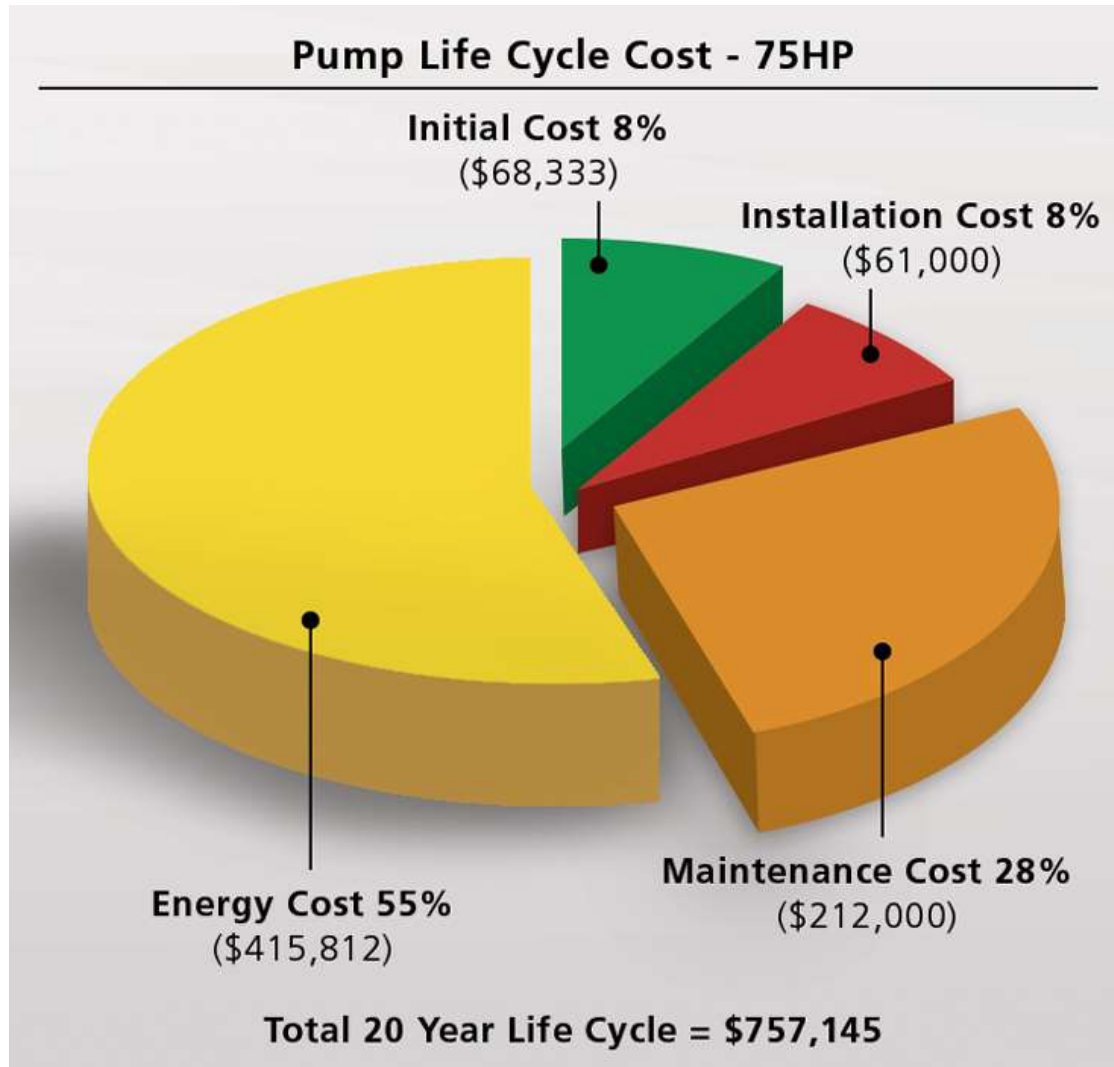


Goals of Presentation

- Identify ways to save energy costs with pumping
- Discuss some interesting case study examples
- Introduce you to DOE's Pumping Assessment Tool

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Typical Life Cycle Costs for a Pump





First, the Pumping System Assessment Tool

- PSAT is a free on-line software tool developed by DOE
- Primarily intended for industrial operations, but can be helpful for water & wastewater utilities

- Uses hydraulic institute standards & measured pump performance data to identify areas where pump efficiencies can be improved

- Specifically, PSAT uses pump and motor performance data from Hydraulic Institute standard ANSI/HI-1.3 and MotorMaster+ database info to estimate existing, achievable performance

(MotorMaster+ is an earlier DOE motor efficiency tool)

- Requires field measurements or estimates of flow rate, pressure, and motor power or current

- Assesses your current pump system operating efficiency by comparing field measurements of power delivered to the motor with the fluid work (flow & head) required by the application

- Can identify the operational cost savings from installing a new pump/pump system

- Is your pump properly sized?
- Is your pump service degraded?
- Do you have an old, inefficient motor?
- Is the pump just operated ineffectively?
- Would installing/modifying a check or control valve change system efficiency?

- Gives you an optimization rating of your existing pump compared to equivalent top line equipment at peak efficiency (i.e., vs a pump with a rating of 100)
- Provides annual energy use and energy costs for existing and revised pump equipment

Condition A

Multistage boiler feed

Pump rpm

3560

Drive

Direct drive

Units

gpm, ft, hp

Kinematic viscosity (cS)

1.00

Specific gravity

0.944

stages

5

Fixed specific speed?

YES

Line freq.

60 Hz

HP

3000

Motor rpm

3560

Eff. class

Energy efficient

Voltage

4160

Estimate FLA

Full-load amps

355.6

Size margin, %

15

Operating fraction

1.000

\$/kwhr

0.0618

Flow rate, gpm

2639

Head tool

Head, ft

2645

Load estim. method

Power

Motor kW

1600.0

Voltage

4160

Retrieve defaults

Set defaults

Copy A > to B >

System curve tool: select below

Condition B

Multistage boiler feed

Pump rpm

3560

Drive

Direct drive

Units

gpm, ft, hp

Kinematic viscosity (cS)

1.00

Specific gravity

0.944

stages

5

Fixed specific speed?

YES

Line freq.

60 Hz

HP

3000

Motor rpm

3560

Eff. class

Energy efficient

Voltage

4160

Estimate FLA

Full-load amps

355.6

Size margin, %

15

Operating fraction

1.000

\$/kwhr

0.0618

Flow rate, gpm

2639

Head tool

Head, ft

2155

Load estim. method

Power

Motor kW

1600.0

Voltage

4160

Copy B < to A <

Background information

STOP

Condition A

Existing

Optimal

Units

Condition B

Existing

Optimal

Units

Pump efficiency	80.8	86.2	%	65.8	86.5	%
Motor rated power	3000	2250	hp	3000	2000	hp
Motor shaft power	2058.5	1930.0	hp	2058.5	1566.4	hp
Pump shaft power	2058.5	1930.0	hp	2058.5	1566.4	hp
Motor efficiency	96.0	96.3	%	96.0	96.2	%
Motor power factor	89.2	90.0	%	89.2	89.5	%
Motor current	249.1	230.5	amps	249.1	188.4	amps
Motor power	1600.0	1494.5	kW	1600.0	1214.7	kW
Annual energy	14016.0	13091.4	MWh	14016.0	10640.5	MWh
Annual cost	866.2	809.0	\$1000	866.2	657.6	\$1000

Annual savings potential, \$1,000

57.1

208.6

Optimization rating, %

93.4

75.9

Log file controls:

Create new log

Add to existing log

Retrieve log entry

Delete log entry

Summary file controls:

Create new summary file

Existing summary files

CREATE NEW

Condition A Notes

Facility

Westvaco

System

Boiler FW Pumps

Date

Nov 25, 2015

Application

Boilers 6 and 7

Evaluator

Cunningham

General comments

Feedwater pump discharge pressure is ~1100 psig. The boiler pressure is maximum of 650 psig. when the pumps are replaced the discharge pressure could be dropped by at least 200 psi, or 490 ft of head. Condition A is the current operation.

Condition B Notes

Facility

System

Date

Application

Evaluator

General comments

The pump head is reduced by 200 psi, or 490 ft of head. The optimal condition is used as the after project condition. Savings are \$208,600/year. This is a costly project and will only be done when the pumps require major maintenance.

Main panel overview

Inputs

Results

Pumping System Assessment Tool

File Tools Help

PSAT 2008

Condition A

End suction stock

Pump rpm: 1185

Drive: Direct drive

Units: gpm, ft, hp

Kinematic viscosity (cS): 1.00

Specific gravity: 1.000

stages: 1

Fixed specific speed? YES

Line freq: 60 Hz

HP: 100

Motor rpm: 1185

Eff. class: Specified (below)

FL efficiency, %: 94.1

Voltage: 480

Estimate FLA

Full load amps: 117.0

Size margin, %: 0

Operating fraction: 0.970

\$/kwhr: 0.0660

Flow rate, gpm: 3210

Head tool: Head, ft: 73.7

Load estim. method: Current

Motor amps: 104.0

Voltage: 473

Rollback defaults

Set defaults

Copy A to B

System curve tool: select below

Condition B

End suction stock

Pump rpm: 1185

Drive: Direct drive

Units: gpm, ft, hp

Kinematic viscosity (cS): 1.00

Specific gravity: 1.000

stages: 1

Fixed specific speed? YES

Line freq: 60 Hz

HP: 100

Motor rpm: 1185

Eff. class: Specified (below)

FL efficiency, %: 94.1

Voltage: 480

Estimate FLA

Full load amps: 117.0

Size margin, %: 0

Operating fraction: 0.970

\$/kwhr: 0.0660

Flow rate, gpm: 3210

Head tool: Head, ft: 22.3

Load estim. method: Current

Motor amps: 104.0

Voltage: 473

Copy B to A

Background information

STOP

Condition A

	Existing	Optimal	Units
Pump efficiency	85.9	85.1	%
Motor rated power	100	75	hp
Motor shaft power	90.6	70.1	hp
Pump shaft power	90.6	70.1	hp
Motor efficiency	94.2	94.5	%
Motor power factor	84.2	82.7	%
Motor current	104.0	81.8	amps
Motor power	71.8	65.4	kW
Annual energy	608.7	470.7	MWh
Annual cost	33.5	25.9	\$1000

Annual savings potential, \$1,000: 7.6

Optimization rating, %: 77.2

Log file controls

Create new log

Retrieve log entry

Assemble existing log

Delete log entry

Summary file controls

Create new summary file

Existing summary files

CREATE NEW

Documentation section

Condition A Notes

Facility: RR

System: Clarified water

Date: 12-18-07

Application: North clarifier, pump measured

Evaluator: DAC

General comments: Pressure from permanently installed gauge, after check valve. Assumed loss is at 2 ft/sec, check notes.

Condition B Notes

Facility: RR

System: Clarified water

Date: 12-18-07

Application: North clarifier, pump measured

Evaluator: DAC

General comments: Developed head minus head loss across level control valve.

Documentation



Doing a PSAT Study can be tricky

- Assemble the right team of people to work on this project



For assistance with PSAT: Team up with these folks

- TVA's Comprehensive Services Program
– Jason Snyder
- Dr. Glenn Cunningham -Tennessee Tech
University
gcunningham@tnitech.edu
- EPA Region 4 – Brendan Held

Work as a team with your Utility electrician

Five Basic Causes of less than optimal pumping system operation

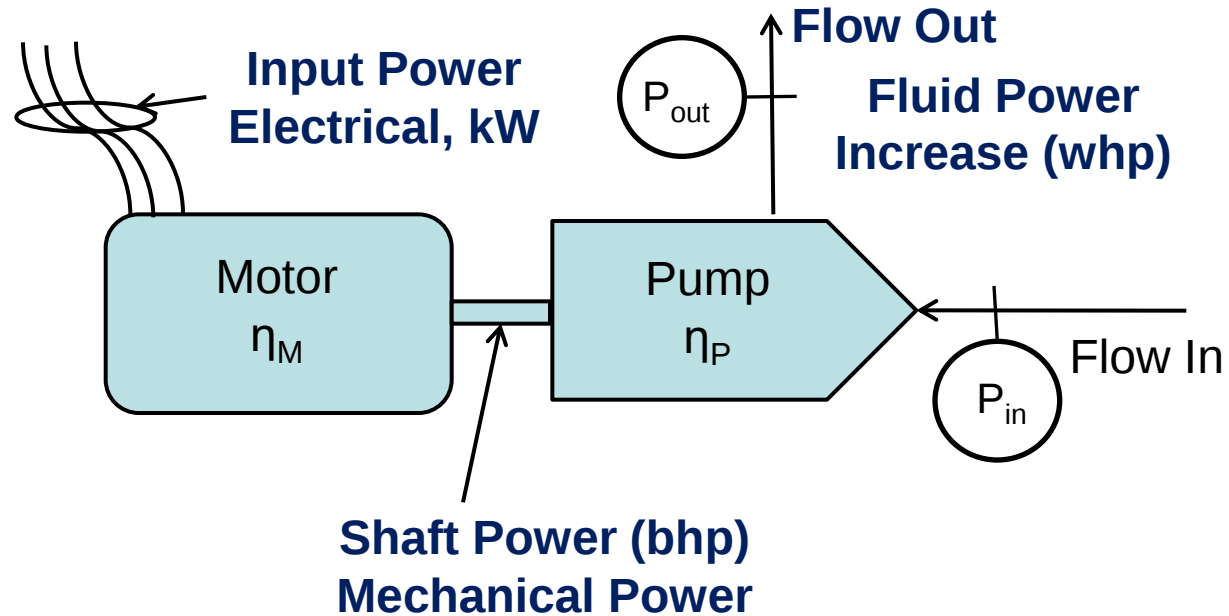
- Installed *components* are inherently inefficient at normal operation conditions
- Installed *components* have degraded in service
- More flow is being provided than the *system* requires
- More head is being provided than the *system* requires
- Equipment is being run when not required by the *system*



Opportunities for Pump Savings

- Throttle valve-controlled systems
- Bypass (recirculation) line normally open
- Multiple parallel pump system with same number of pumps always operating
- Constant pump operation in a batch environment or frequent cycle batch operation in a continuous process
- Cavitation noise (at pump or elsewhere in the system)
- High system maintenance
- Systems that have undergone change in function
- Pumping at higher flow rates than are necessary for shorter periods of time

Pumping Power Diagram



$$\text{Shaft Power (bhp)} = \text{Motor Input Power} * (\eta_M)$$

$$\text{Fluid Energy Increase (whp)} = \text{Shaft Power (bhp)} * (\eta_P)$$

$$(1 \text{ HP} = 0.746 \text{ kW})$$



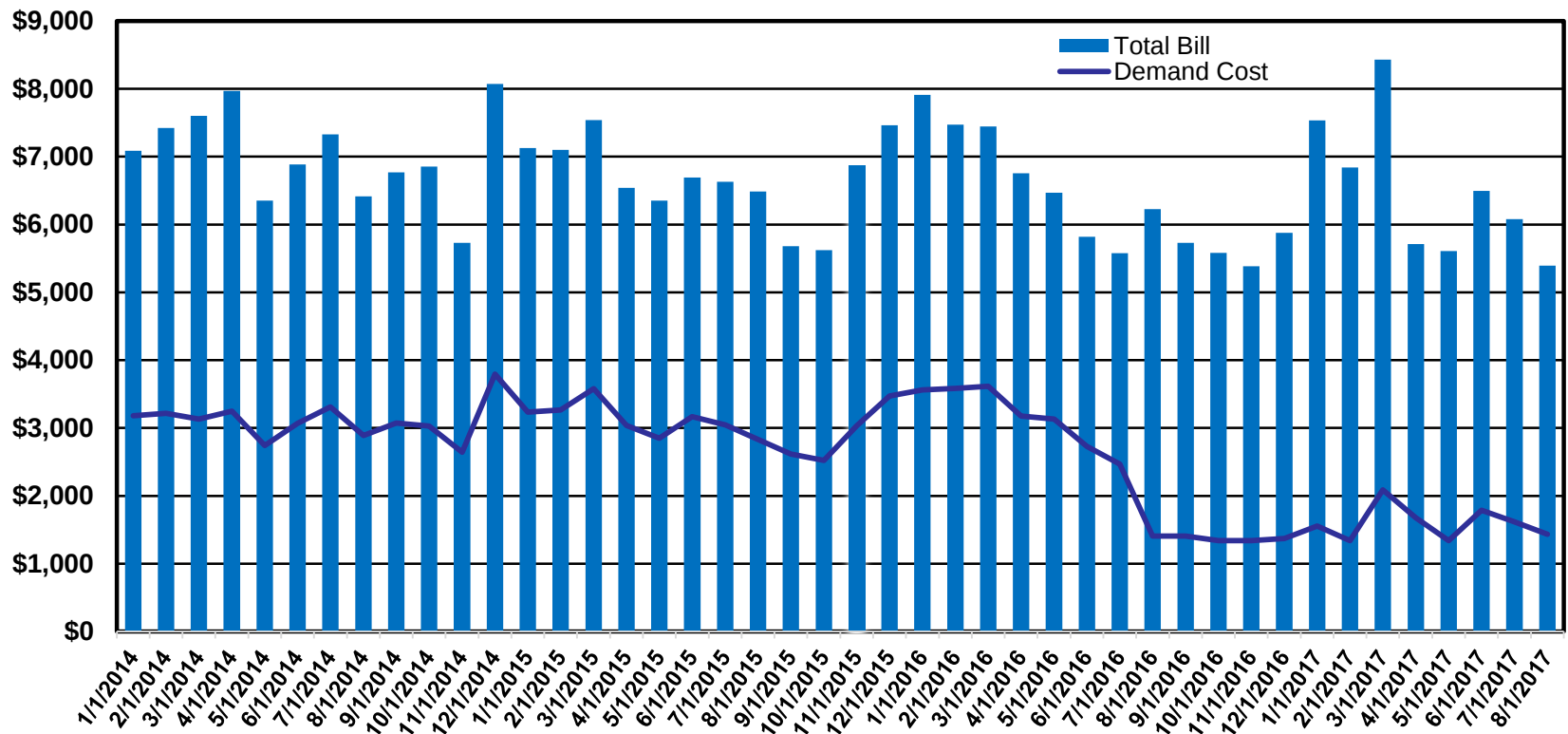
Power Costs are Increasing

- Case in Point: One Alabama utility reduced power usage by 38% in 2017 but only saw a 9% cost savings because power costs increased \$49% since 2014...!!



The effect of Demand charges

Hanceville WWTP - AL0057029
Monthly Power Bills \$\$/Month



The effect of Demand charges

- So Hanceville saw a \$2,100 decrease in its monthly **demand** charge over a 6 month period
- Some of this savings was due to installing a VFD on its main influent WWTP pumps

- Flow is proportional to shaft speed
- Head (pressure) is proportional to the square of shaft speed
- Power is proportional to the cube of shaft speed

$$\frac{Q_1}{Q_2} = \left(\frac{N_1}{N_2} \right)$$

Flow

$$\frac{H_1}{H_2} = \left(\frac{N_1}{N_2} \right)^2$$

Pressure

$$\frac{P_1}{P_2} = \left(\frac{N_1}{N_2} \right)^3$$

Power

- On average, 80% of the time pumps operate at 60% of their full capacity
[Source: Baldor Motors]

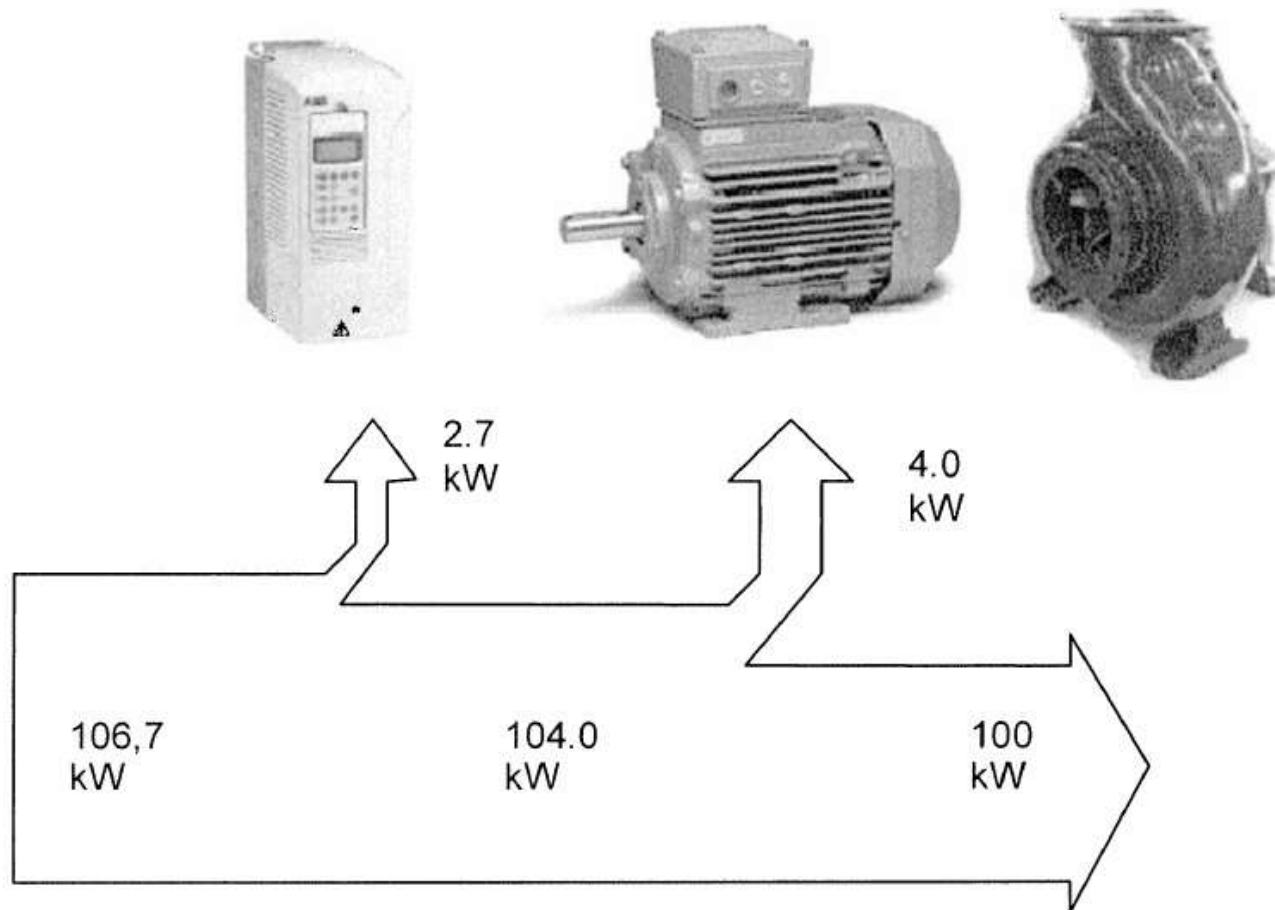
This indicates there is often an opportunity to save energy by controlling pump operation

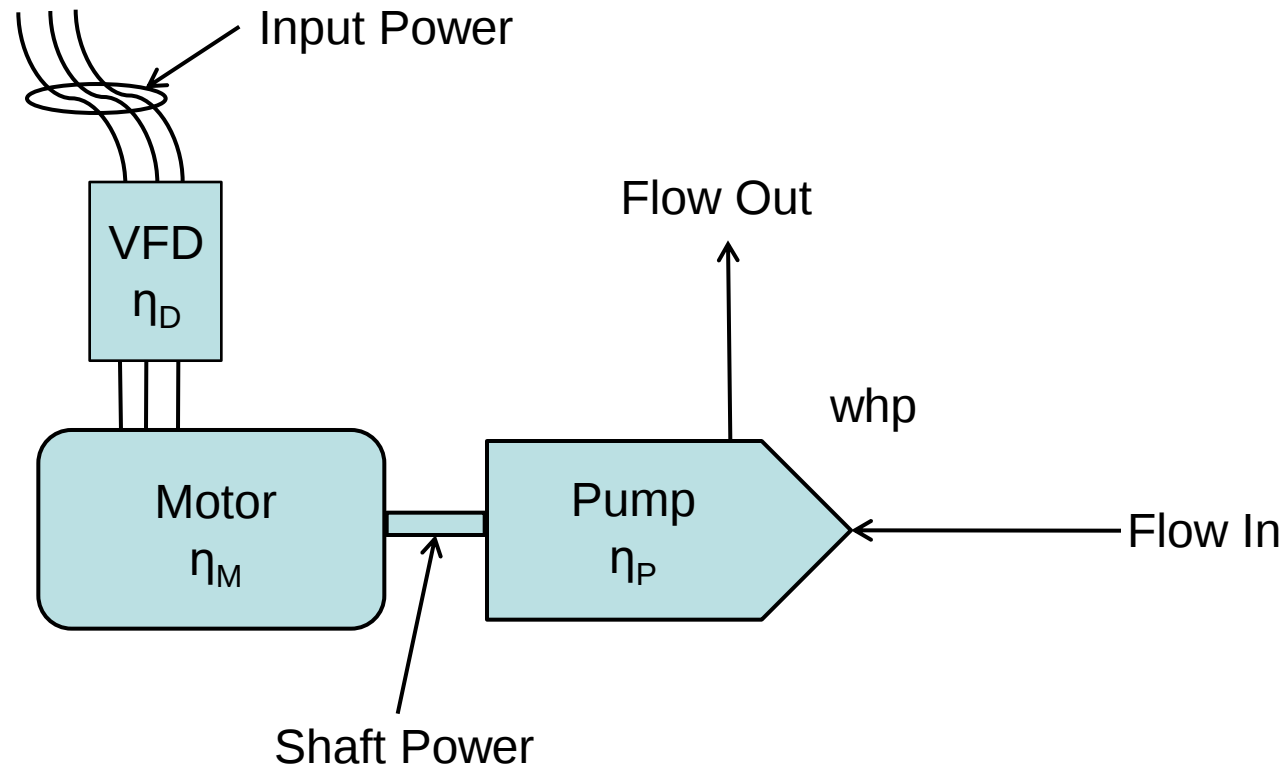
Where warranted, A VFD Can:

- **Provide improved process control**
- **Save electrical energy**
- **Reduce wear and tear on equipment**

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AC Drive and Motor Losses





$$\text{VFD Input Power} = \text{whp} / (\eta_D * \eta_M * \eta_P)$$

- Generates Heat (2-3 % loss)
- Generate harmonics (current distortion)

So, a VFD adds a degree of inefficiency

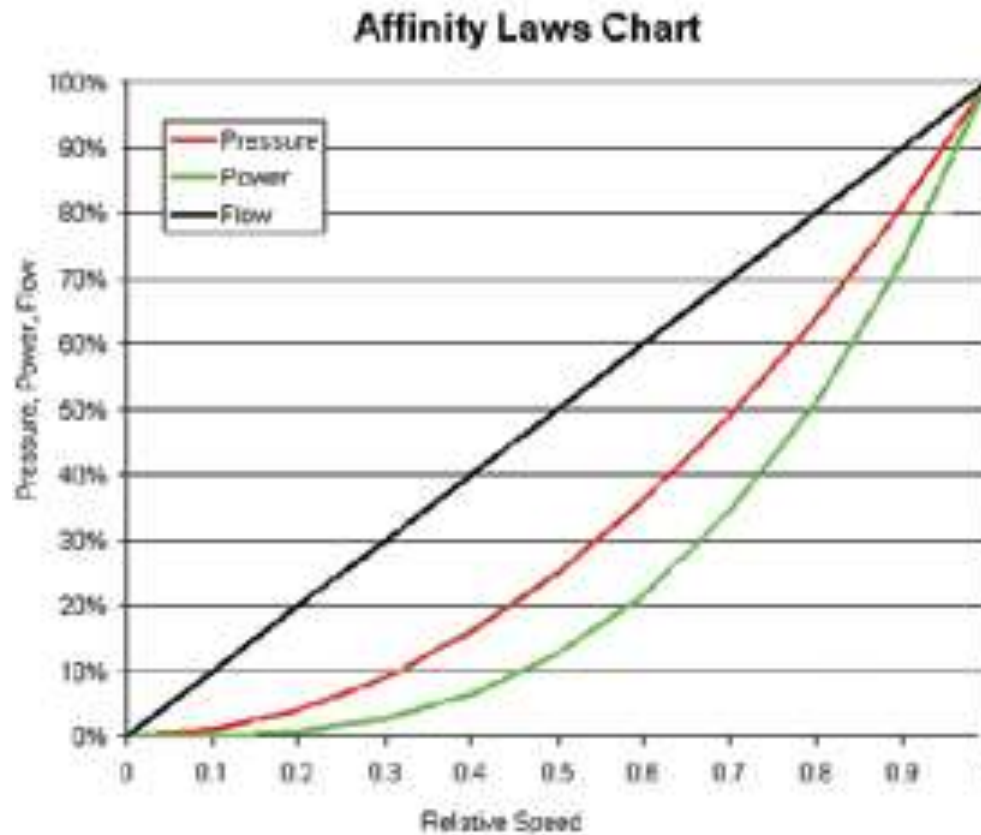
- VFDs save energy by using less overall power
 - Power a pump consumes is proportional to the cube of velocity. Theoretically, if you run a pump at 80% speed, you can save 51% of full load power)
- VFDs run at a high power factor- Results in potential cost savings and increase in motor life



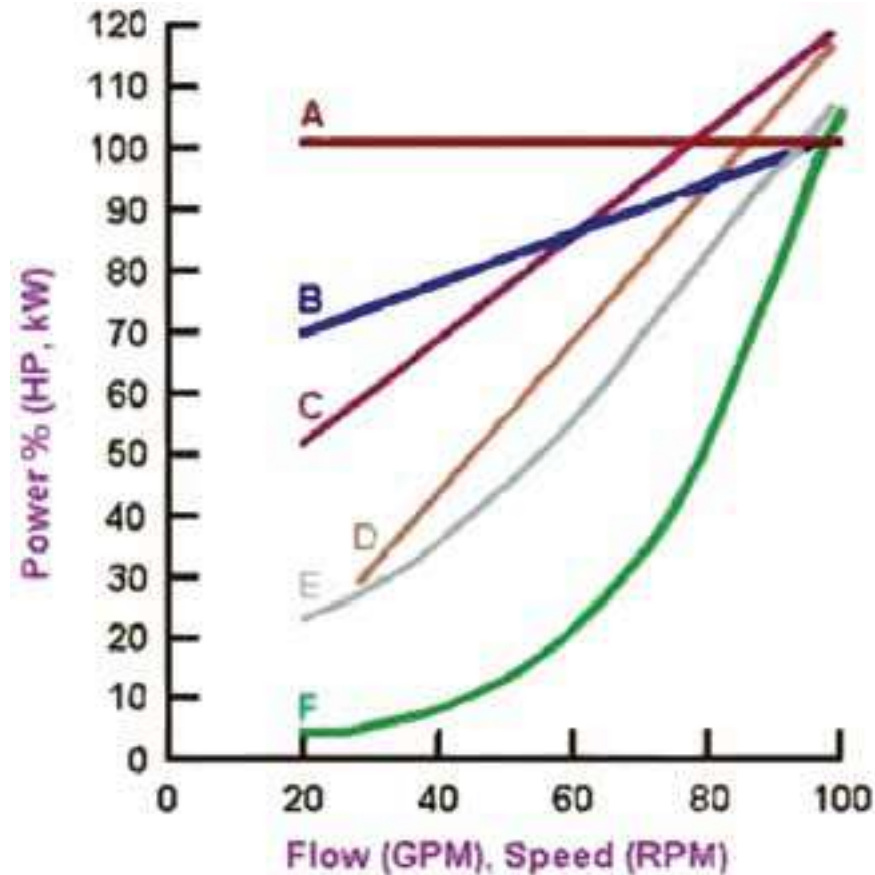
Theoretical Power Savings

- Running a pump at 60% of its operating volume requires only 22% input power

Volume	Pressure/Head	HP Required
100%	100%	100%
80%	64%	51%
60%	36%	22%
40%	16%	6%



- Curve A – Diverting Valve
- Curve B – Throttling Valve
- Curve C – Hydrostatic Drive
- Curve D – Mechanical Drive
- Curve E – Eddy Current Clutch
- Curve F – Variable Speed Drive



- Comes closest to achieving the theoretical maximum efficiency of a pump

For a centrifugal pump:

- An adjustable AC drive can save a great deal of energy if a pump is designed to operate at somewhere between 40-80 % speed
- Savings: 10 to 60 %



Power/Demand Fee Structure Trend

TVA – Lower unit power cost but higher demand charge

Southern Company – Higher unit power cost but lower demand charge



Example Usage/Demand Charge

Lift Station Pump: 200 hp, Single Speed
Centrifugal Pump

Utility Costs: \$14.36/kW Demand Charge

This pump runs for ten 30-min cycles/day



Example: Energy Usage Cost

Energy Cost:

Pumping at 92% efficiency

Lift Station Pump: 200 hp, Single Speed
Centrifugal Pump



Energy Consumed

Unit Cost of \$0.10/kWh

Pumping at 92% efficiency

Energy Use:

$200 \text{ hp} \times 0.746 \text{ kW/hp} \times 5 \text{ hr/day} \times 30 \text{ days/mo} \times 0.92 = 20,600 \text{ kWh/Mo}$



Energy Usage Cost

$$\begin{aligned}\text{Energy Cost} &= 20,600 \text{ kWh/Mo} \times \$0.10/\text{kWh} \\ &= \$2,060/\text{Month}\end{aligned}$$



Example Demand Charge

For the short cycle time, the operation of this pump imparts a significant demand charge on the utility:

$$200 \text{ hp} \times 0.7457 \text{ kW/hp} = 149 \text{ kW}$$

The demand cost to run this pump:

$$149 \text{ kW} \times \$14.36/\text{kW} = \$2,140/\text{Month}$$



Example Demand Charge

So, the utility is paying:

\$2,060/Month in Energy Usage

AND

\$2,140/Month in Demand Charge

To run this pump



What Can be done...?

The utility can install a variable frequency drive (VFD) on the pump:

Conceivably, the pump may then begin a pump cycle at 40% speed and increase to 60% speed. It may never need to run $> 85\%$ speed or it may pump at 100% speed for < 15 min per cycle (typ SCADA-controlled).



What Can be done...?

Anything that runs < 15 minutes won't show up as a demand charge

Note: Your Demand period may be 15 min or 30 min.



What Can be done...?

Say the average pump run speed is now 50% and the pump now operates for double the amount of time:

Drive efficiency would decrease somewhat:
...say 5%



What Can be done...?

Energy Usage:

$$\begin{aligned} &0.13 \times 200 \text{ hp} \times 0.746 \text{ kW/hp} \times 10 \text{ hr/day} \times \\ &30 \text{ days/mo} \times 0.92 \times 1.05 \\ &= 5,600 \text{ kWh/Mo} \end{aligned}$$

$$\begin{aligned} \text{Energy Cost: } &5,600 \text{ kWh/Mo} \times \$0.10/\text{kWh} \\ &= \$560/\text{Month (73\% savings)} \end{aligned}$$

** Efficiency roughly estimated



What Can be done...?

Demand Usage:

$$200 \text{ hp} \times 0.13 \times 0.746 \text{ kW/hp} = 19.4 \text{ kW}$$

(decrease from 149 kW)

Demand Charge: $19.4 \text{ kW} \times \$14.36/\text{kW}$
 $= \$280/\text{Month}$
(87% savings)



Resulting Savings from VFD Installation

So the utility is now paying quite a bit less to operate the pump from: \$2,060 to \$560/Month

But they have also reduced the demand cost from \$2,140 to \$280/month:

That's a net monthly savings of **\$3,360/Month**



Resulting Savings from VFD Installation

A savings of 80%..!! BUT, if this electric utility only charges a demand cost for a certain kW threshold, conceivably, the entire demand cost of this pump may be eliminated: a net savings of:

\$3,640/Month...!! (87% Savings)

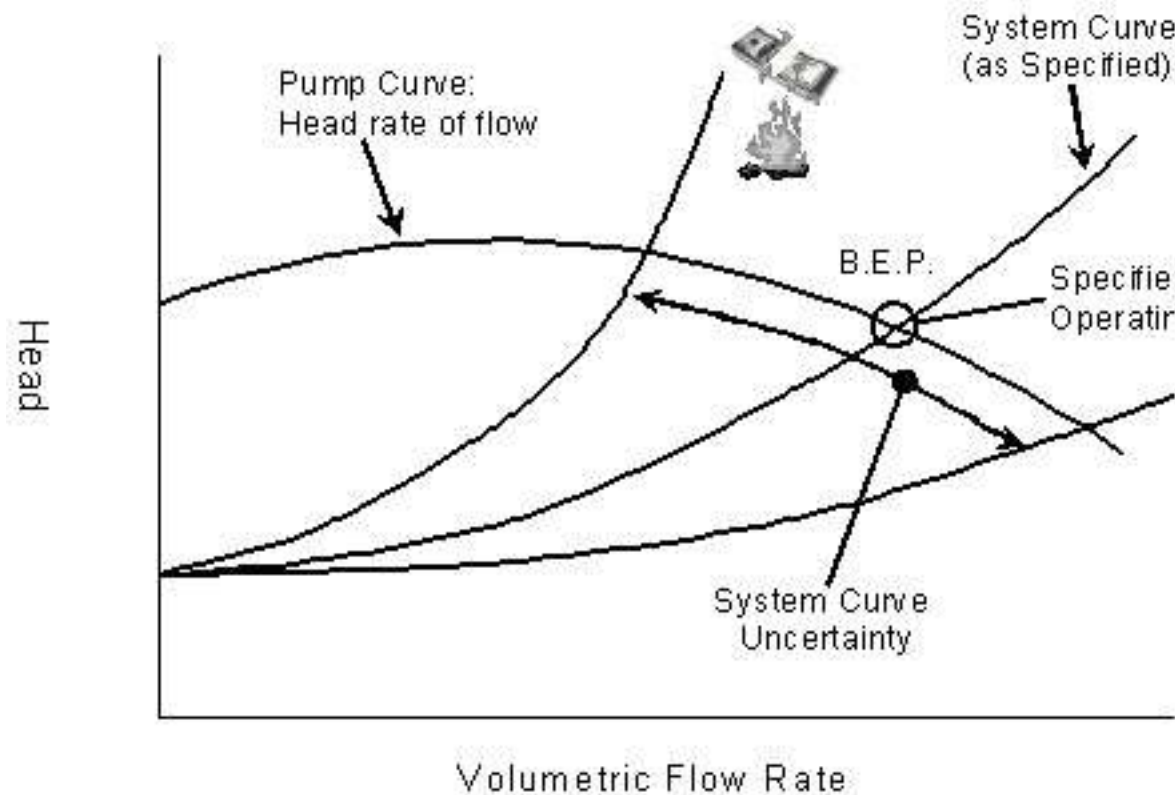
(Note: There may be a base demand charge)



VFDs can be expensive

- But in many applications, the payback period is < 2 years
- And annual cost savings continue..!

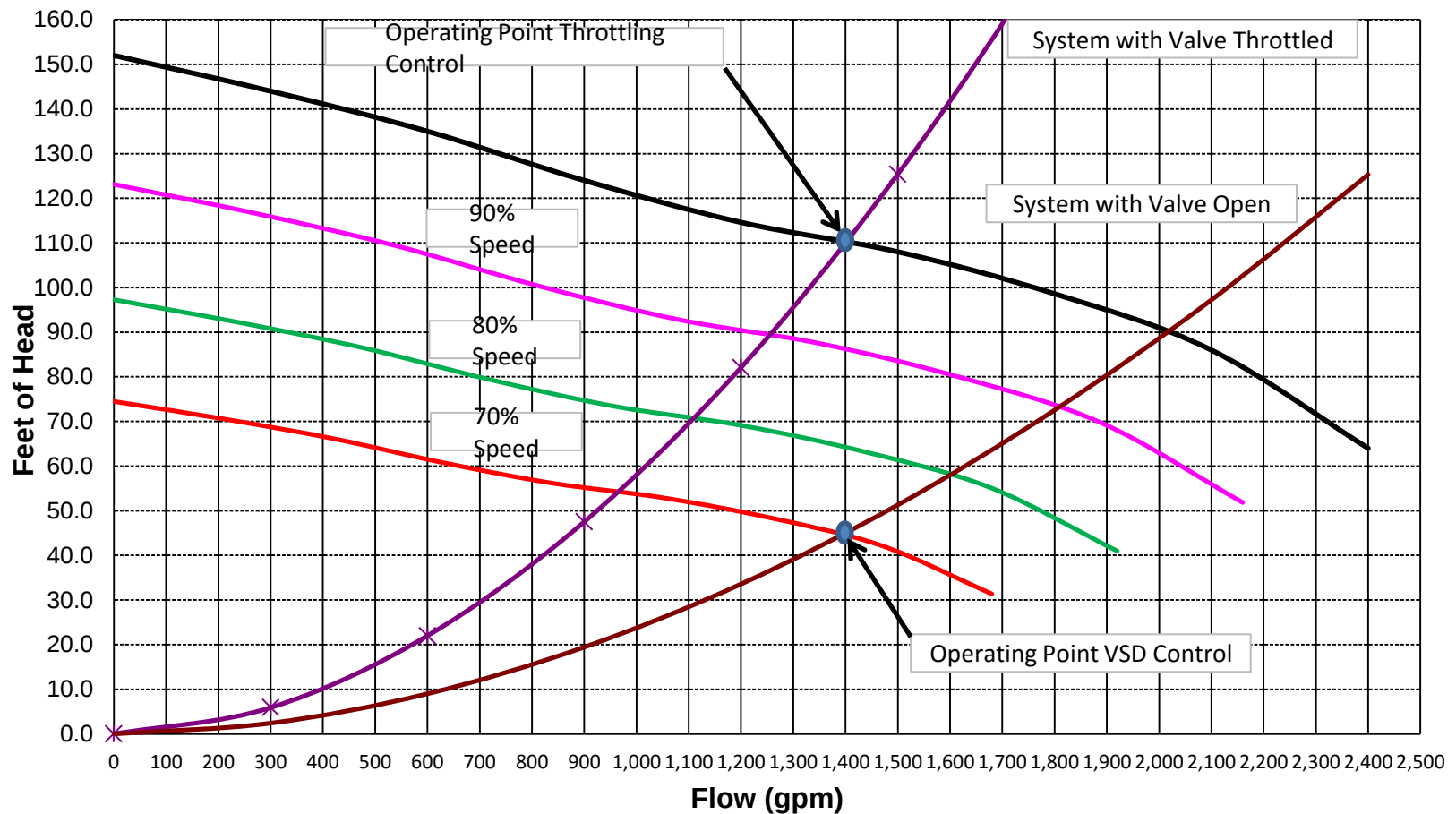
Need to Check Pump System Condition



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Ensure a VFD is the right “System” Solution

Variable Speed Pumping





You need to assess each site-specific Application

Determine if the pump design and system design will facilitate reliable control & operation by using a VFD for turndown

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OK...so this is a fan
company



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**But if you have a REALLY
big pump...**

It warrants a close look

Questions..?

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